being 0.1 to 1.0 mm and smaller than crystalline material produced by the mass crystallization, and introducing the seeding product into the crystallizer while maintaining temperature thereof up to 40°C lower than the temperature of the crystallization medium, all other materials fed or recycled into the crystallizer being free of solids.

8. A method according to claim 7, wherein the crystallization is of ammonium sulfate.

9. A method according to claim 7 or 8, wherein said temperature of the seeding product is 10 to 30°C lower than the temperature of the crystallization medium.

10. A method according to claim 3, wherein the amount of the seeding product introduced into the crystallizer based on the solids discharged from the crystallizer is 7 to 15% by weight.

11. A method according to claim 7 or 8, wherein the solids of the seeding product are produced by a separate crystallization.--

Amend claims 2-6 as follows, the amendments being shown by brackets and underlining in the Appendix hereto:

A2

2. (Amended) A method according to claim 7, wherein the seeding product is introduced into the crystallizer discontinuously in such a manner that the proportion by weight of a selected fraction of the crystalline material in the crystallizer is maintained within predetermined limits.

3. (Amended) A method according to claim 7, wherein the seeding product is introduced into the crystallizer continuously and the solids of the seeding product are introduced into the crystallizer in amounts of 5 to 30% by weight based on solids discharged from the crystallizer.

4. (Amended) A method according to claim 7 or 8, wherein the average particle diameter of the solids of the seeding product is 0.3 to 0.8 mm.

5. (Amended) A method according to claim 7 or 8, wherein the solids of the seeding product are produced by mechanical communition of crystals produced by the mass crystallization.